

From Quasi-Geostrophy to Boussinesq Dynamics and In-Between

Leslie Smith
UW - Madison

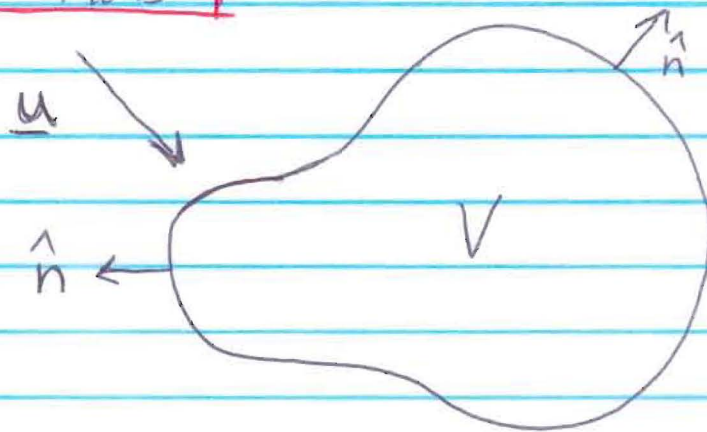
- ① Derivation of the Boussinesq Equations
- ② Linear and nonlinear structure in terms of waves
- ③ Traditional and alternative derivations of the Quasi-Geostrophic Equations
- ④ Reduced models "in between"

NCAR/IMAGE Summer Workshop Lecture 1

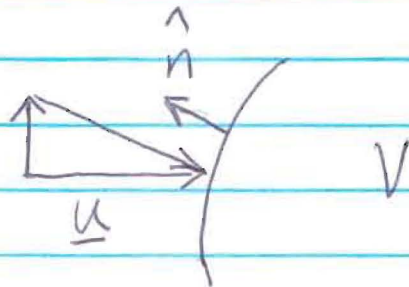
Derivation of the Boussinesq approximation from the conservation laws governing continuum fluid dynamics.

Conservation of Mass

$\rho(\underline{x}, t)$
is density



$$\frac{d}{dt} \int_V \rho dV = \frac{\text{mass in} - \text{mass out}}{\text{unit time}} = \int_A \rho (-\underline{u} \cdot \hat{n}) dA$$



Divergence Thm:
$$\int_V \underline{\nabla} \cdot \underline{F} dV = \int_A \underline{F} \cdot \hat{n} dA$$

$$\frac{d}{dt} \int_V \rho dV = - \int_V \nabla \cdot (\rho \underline{u}) dV$$

Shrink the volume to a point \Rightarrow

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{u}) = 0 \quad \text{or} \quad \frac{D\rho}{Dt} = -\rho \nabla \cdot \underline{u}$$

$$\frac{D}{Dt} = \frac{\partial}{\partial t} + \underline{u} \cdot \nabla$$

Conservation of Momentum $\underline{F} = m \underline{a}$

$$\frac{d}{dt} \int_V \rho \underline{u} dV = \frac{\text{momentum in} - \text{momentum out}}{\text{unit time}} + \underline{F}$$

$$= \int_A \rho \underline{u} (-\underline{u} \cdot \hat{n}) dA + \underline{F}$$

$$= \int_V -\nabla \cdot (\rho \underline{u} \underline{u}) dV + \underline{F}$$

Shrink the volume to a point \Rightarrow

$$\frac{\partial}{\partial t} (\rho \underline{u}) + \nabla \cdot (\rho \underline{u} \underline{u}) = \underline{F}' \quad \left(\begin{array}{l} \text{per unit} \\ \text{volume} \end{array} \right)$$

$$\frac{d}{dt}(\rho \underline{u}) + \underline{u} \cdot \nabla (\rho \underline{u}) + \rho \underline{u} (\nabla \cdot \underline{u}) = \underline{F} \quad (\text{drop prime})$$

$$\frac{D}{Dt}(\rho \underline{u}) + \rho \underline{u} (\nabla \cdot \underline{u}) = \underline{F}$$

$$\rho \frac{D\underline{u}}{Dt} + \underline{u} \frac{D\rho}{Dt} + \rho \underline{u} (\nabla \cdot \underline{u}) = \underline{F}$$

use Conservation of Mass $\frac{D\rho}{Dt} = -\rho \nabla \cdot \underline{u}$

$$\rho \frac{D\underline{u}}{Dt} - \rho \underline{u} \nabla \cdot \underline{u} + \rho \underline{u} \nabla \cdot \underline{u} = \underline{F}$$

$$\rho \frac{D\underline{u}}{Dt} = \underline{F}$$

What is \underline{F} ?

Body Forces

$\left[\frac{\text{Force}}{\text{volume}} \right]$ gravity $\rho \underline{g}$

Surface Forces

$\left[\frac{\text{force}}{\text{area}} \right]$

normal and tangential stresses

$$\underline{F}_s = \underline{\nabla} \cdot \underline{\sigma} = -\underline{\nabla} p + \underline{\nabla} \cdot \underline{\tau}$$

$$\underline{\sigma} = -p \underline{I} + \underline{\tau}$$

p is the compressive-normal stress at any point in a fluid at rest

$\underline{\tau}$ gives additional tensile-normal and tangential stresses at a point in a fluid in motion

$\underline{\tau}$ symmetric follows from conservation of angular momentum

For a Newtonian Fluid

$$\underline{\tau} = \lambda \text{Tr}(\underline{S}) \underline{I} + 2\mu \underline{S}$$

$$* \quad \underline{S} = \frac{1}{2} \left[\underline{\nabla} \underline{u} + (\underline{\nabla} \underline{u})^T \right]$$

symmetric part of the strain rate

$$\text{Tr}(\underline{S}) = \underline{\nabla} \cdot \underline{u}$$

* λ, μ can be different] [think of adding purely compressive additional stresses]

Consider the sum of all the normal stresses

$$\text{Tr}(\underline{\underline{\sigma}}) = -3p + 3\lambda \text{Tr}(\underline{\underline{S}}) + 2\mu \text{Tr}(\underline{\underline{S}})$$

$$p - \frac{1}{3} \text{Tr}(\underline{\underline{\sigma}}) = \left(\frac{2}{3} \mu + \lambda \right) \nabla \cdot \underline{u}$$

The quantity $\left(\frac{2}{3} \mu + \lambda \right)$ is measured to be significantly different from zero only when compressibility effects are very strong, e.g. when shock waves are present.

Stokes assumption: $\lambda = -\frac{2}{3} \mu \Rightarrow$

$$\underline{\underline{\sigma}} = -p \underline{\underline{I}} + 2\mu \underline{\underline{S}} - \frac{2}{3} \mu (\nabla \cdot \underline{u}) \underline{\underline{I}}$$

$$\underline{F}_s = \nabla \cdot \underline{\underline{\sigma}} = -\nabla \left[p + \frac{2}{3} \mu \nabla \cdot \underline{u} \right] + \nabla \cdot (2\mu \underline{\underline{S}})$$

μ = coefficient of viscosity

So far 4 equations, 5 unknowns

u, v, w, p, ρ

Assume an ideal gas with $\rho = \rho RT$
 and the Thermal Energy Equation \Rightarrow
 6 equations, 6 unknowns

1st Law of Thermodynamics

Fluid at rest: $\delta Q = d\hat{u} + \delta W$

heat added to CV \nearrow δQ \nearrow $d\hat{u}$ \nwarrow δW work done by CV
 change in internal energy

Fluid in motion: $\delta Q = d\left(\hat{u} + \frac{\underline{u} \cdot \underline{u}}{2}\right) + \delta W$

Energy Equation (thermal + kinetic)

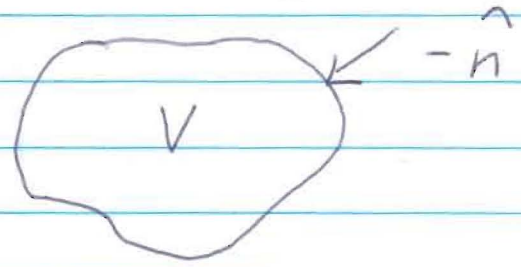
$$\frac{d}{dt} \int_V \rho \left(\hat{u} + \frac{\underline{u} \cdot \underline{u}}{2} \right) dV = \int_A \rho \left(\hat{u} + \frac{\underline{u} \cdot \underline{u}}{2} \right) (-\underline{u} \cdot \hat{n}) dA$$

$\frac{\delta Q}{\delta t}$ \nearrow heat added to CV per unit time

$-\frac{\delta W}{\delta t}$ \nwarrow work done by CV per unit time

work has units of Force \cdot velocity

Work done on CV
by pressure forces



$$\int_A p (-\hat{n}) \cdot \underline{u} dA$$

Work done by CV is $\int_A p \hat{n} \cdot \underline{u} dA$

Pressure $-\frac{\delta W}{\delta t} = -\int_A p \hat{n} \cdot \underline{u} dA$

Viscous Forces $-\frac{\delta W}{\delta t} = \int_A \underline{\underline{\tau}} : \underline{u} \hat{n} dA$

$$\left[\int_A \tau_{ij} u_i n_j dA \right]$$

Gravity $-\frac{\delta W}{\delta t} = \int_V \rho \underline{g} \cdot \underline{u} dV$

Heat added
to CV/unit time

$$\frac{\delta Q}{\delta t} = \int_A \underline{q} \cdot (-\hat{n}) dA$$

\underline{q} is the heat flux vector

Use Divergence Thm. \implies shrink CV to a point

$$\begin{aligned} & \frac{\partial}{\partial t} \left[\rho \left(\hat{u} + \frac{\underline{u} \cdot \underline{u}}{2} \right) \right] + \underline{\nabla} \cdot \left[\rho \left(\hat{u} + \frac{\underline{u} \cdot \underline{u}}{2} \right) \underline{u} \right] \\ &= -\underline{\nabla} \cdot (p \underline{u}) + \underline{\nabla} \cdot [\underline{u} \cdot \underline{\tau}] - \underline{\nabla} \cdot \underline{q} + \rho \underline{q} \cdot \underline{u} \end{aligned}$$

But we know:

$$\frac{\partial}{\partial t} (\rho F) + \underline{\nabla} \cdot (\rho F \underline{u}) = \rho \frac{DF}{Dt}$$

Using vector identities and Conservation of Mass \implies

$$\begin{aligned} \rho \frac{D}{Dt} \left[\hat{u} + \frac{\underline{u} \cdot \underline{u}}{2} \right] &= -\underline{\nabla} \cdot (p \underline{u}) + \underline{\nabla} \cdot [\underline{u} \cdot \underline{\tau}] \\ &\quad - \underline{\nabla} \cdot \underline{q} + \rho \underline{q} \cdot \underline{u} \end{aligned}$$

Subtract off equation for Mechanical
(kinetic) energy which has no new info:

$$\underline{u} \cdot \rho \frac{D\underline{u}}{Dt} = \underline{u} \cdot \left[-\underline{\nabla} p + \rho \underline{g} + \underline{\nabla} \cdot \underline{\underline{T}} \right]$$

$$\rho \frac{D\left(\frac{\underline{u} \cdot \underline{u}}{2}\right)}{Dt} = -\underline{u} \cdot \underline{\nabla} p + \rho \underline{g} \cdot \underline{u} + \underline{u} \cdot \left[\underline{\nabla} \cdot \underline{\underline{T}} \right]$$

After the subtraction:

$$\rho \frac{D\hat{u}}{Dt} = -p \underline{\nabla} \cdot \underline{u} - \underline{\nabla} \cdot \underline{q} + \underline{\underline{T}} : \underline{\nabla} \underline{u}$$

is the thermal energy equation

Summary Newtonian Fluid $\underline{T} \propto \underline{S}$;

Stokes assumption $\lambda = -\frac{2}{3}\mu$; Ideal Gas

$$* \frac{D\rho}{Dt} + \rho \nabla \cdot \underline{u} = 0, \quad * p = \rho RT$$

$$* \rho \frac{D\underline{u}}{Dt} = \rho \underline{g} - \nabla \left[p + \frac{2}{3} \mu \nabla \cdot \underline{u} \right] + \nabla \cdot (2\mu \underline{S})$$

$$= \rho \underline{g} - \nabla p + \nabla \cdot \underline{T}$$

$$* \rho \frac{D\hat{u}}{Dt} = -\rho \nabla \cdot \underline{u} - \nabla \cdot \underline{q} + \underline{T} : \nabla \underline{u}$$

$$\underline{T} = 2\mu \underline{S} - \frac{2}{3}\mu \nabla \cdot \underline{u} \underline{I}$$

$$\underline{S} = \frac{1}{2} \left[\nabla \underline{u} + (\nabla \underline{u})^T \right]$$

\underline{q} = heat flux vector, μ = coefficient of viscosity

6 equations, 6 unknowns $\underline{u}, \rho, p, T$

if \underline{q} is given in terms of T

The Boussinesq Approximation

Thermal Heat Equation:

$$\rho \frac{D\hat{u}}{Dt} = -\underline{\nabla} \cdot \underline{q} - p \underline{\nabla} \cdot \underline{u} + \underline{\underline{T}} : \underline{\nabla} \underline{u}$$

In general $-p \underline{\nabla} \cdot \underline{u} = \frac{p}{\rho} \frac{D\rho}{Dt}$

Now assume ρ depends mainly on T
 [neglect dependence on p and salt]

$$\begin{aligned} -p \underline{\nabla} \cdot \underline{u} &= \frac{p}{\rho} \frac{D\rho}{Dt} \approx \frac{p}{\rho} \left. \frac{\partial \rho}{\partial T} \right|_p \frac{DT}{Dt} \\ &= -p \alpha \frac{DT}{Dt} \end{aligned}$$

with $\alpha = -\frac{1}{\rho} \left. \frac{\partial \rho}{\partial T} \right|_p$ is the thermal

expansion coefficient; dimension $\frac{1}{T} [^{\circ}\text{K}]$

By Ideal Gas Law $p = \rho RT$

$$\alpha = -\frac{1}{\rho} \left. \frac{\partial \rho}{\partial T} \right|_p = -\frac{1}{\rho} \left(\frac{-p}{RT^2} \right) = \frac{1}{T}$$

$$\text{So } -\rho \underline{\nabla} \cdot \underline{u} \approx -\frac{\rho RT}{T} \frac{DT}{Dt} = -\rho (c_p - c_v) \frac{DT}{Dt}$$

[see handout]

with $\hat{u}(T) = c_v T$ [see handout] and

neglecting viscous heating \Rightarrow

$$\rho \frac{D}{Dt} (c_v T) \approx -\underline{\nabla} \cdot \underline{q} - \rho (c_p - c_v) \frac{DT}{Dt}$$

$$\Rightarrow \rho c_p \frac{DT}{Dt} = -\underline{\nabla} \cdot \underline{q}$$

Finally Fourier's law of Heat Conduction

$$\Rightarrow \rho c_p \frac{DT}{Dt} = -\underline{\nabla} \cdot [-k \underline{\nabla} T] = k \nabla^2 T$$

Now assume the background state ρ_0, T_0 is in hydrostatic balance

$$\rho = \rho_0 + \tilde{\rho}(x, t), \quad |\tilde{\rho}| \ll \rho_0$$

$$T = T_0 + \tilde{T}(x, t)$$

$$p = p_0(z) + \tilde{p}(x, t); \quad \nabla p_0(z) = \rho_0 g$$

$$\frac{\partial \rho}{\rho} \approx -\alpha \partial T \quad \text{and} \quad |\tilde{\rho}| \ll \rho_0 \implies$$

$$\frac{\rho - \rho_0}{\rho_0} \approx -\alpha (T - T_0) \quad \text{or} \quad -\frac{\tilde{\rho}}{\alpha \rho_0} \approx \tilde{T}$$

Thermal Energy

$$\rho_0 c_p \frac{DT}{Dt} = k \nabla^2 T \implies$$

$$\rho_0 c_p \left(\frac{-1}{\alpha \rho_0} \right) \frac{D\tilde{\rho}}{Dt} \approx k \left(\frac{-1}{\alpha \rho_0} \right) \nabla^2 \tilde{\rho} \quad \text{or}$$

$$\frac{D\tilde{\rho}}{Dt} \approx \mathcal{K} \nabla^2 \tilde{\rho}; \quad \mathcal{K} = \frac{k}{\rho_0 c_p}$$

$$\boxed{\text{Mass}} \quad \frac{\partial \rho}{\partial t} + \rho \nabla \cdot \underline{u} + \underline{u} \cdot \nabla \rho = 0$$

$$\frac{\partial \tilde{\rho}}{\partial t} + (\rho_0 + \tilde{\rho}) \nabla \cdot \underline{u} + \underline{u} \cdot \nabla \tilde{\rho} = 0$$

with dominant balance $\boxed{\nabla \cdot \underline{u} = 0}$

$$\boxed{\text{Momentum}} \quad (\rho_0 + \tilde{\rho}) \frac{D\underline{u}}{Dt} = -\nabla [\rho_0(z) + \tilde{p}] + (\rho_0 + \tilde{\rho}) \underline{g} + \nabla \cdot \left[2\mu \underline{S} - \frac{2}{3} \mu \nabla \cdot \underline{u} \underline{I} \right]$$

Subtract $-\nabla \rho_0(z) + \rho_0 \underline{g} = 0$ } \Rightarrow
 use $\nabla \cdot \underline{u} = 0$

$$\left(1 + \frac{\tilde{\rho}}{\rho_0}\right) \frac{D\underline{u}}{Dt} = -\frac{1}{\rho_0} \nabla \tilde{p} + \frac{\tilde{\rho}}{\rho_0} \underline{g} + \frac{\mu}{\rho_0} \nabla^2 \underline{u}$$

with dominant balance

$$\boxed{\frac{D\underline{u}}{Dt} = -\frac{1}{\rho_0} \nabla \tilde{p} + \frac{\tilde{\rho}}{\rho_0} \underline{g} + \frac{\mu}{\rho_0} \nabla^2 \underline{u}}$$

$|\underline{g}| \gg \left| \frac{D\underline{u}}{Dt} \right|$, viscous effects allowed to be large

Summary

$$\nabla \cdot \underline{u} = 0 \quad (\text{mass})$$

$$\rho_0 \frac{D\underline{u}}{Dt} = -\nabla \tilde{p} + \tilde{\rho} \underline{g} + \nu \nabla^2 \underline{u} \quad (\text{momentum})$$

$$\frac{D\tilde{e}}{Dt} = \kappa \nabla^2 \tilde{e} \quad (\text{thermal energy})$$

with background state

$$\rho = \rho_0 + \tilde{\rho}, \quad |\tilde{\rho}| \ll \rho_0$$

$$T = T_0 + \tilde{T}$$

$$p = p_0(z) + \tilde{p}$$

$$\nabla p_0(z) = \rho_0 \underline{g}$$

$$\tilde{e} \approx \alpha \rho_0 (T - T_0)$$

Homework

* Assume another layer of hydrostatic balance

$$\tilde{q} = \rho_1(z) + \rho'(x,t) = -bz + \rho'(x,t)$$

$$\tilde{p} = p_1(z) + p'(x,t)$$

$$\text{with } -\frac{1}{\rho_0} \nabla p_1(z) = \frac{bz}{\rho_0} g, \quad g = -g \hat{z}$$

* Move into the rotating frame $\underline{\Omega} = \Omega \hat{z}$

* Define $\rho' = \left(\frac{b\rho_0}{g}\right)^{1/2} \theta$, $N = \left(\frac{gb}{\rho_0}\right)^{1/2}$

$$P = p'/\rho_0 \quad \Rightarrow$$

$$\nabla \cdot \underline{u} = 0,$$

$$\frac{D\underline{u}}{Dt} + 2\Omega \hat{z} \times \underline{u} + N\theta \hat{z} = -\nabla P + \nu \nabla^2 \underline{u}$$

$$\frac{D\theta}{Dt} - N(\underline{u} \cdot \hat{z}) = \kappa \nabla^2 \theta$$

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Shortcomings of Boussinesq and what to do about it:

- * In the compressible atmosphere, ρ depends on p as well as T
- * Density ρ decreases with height as pressure p decreases
- * The natural background state is not constant density ρ_0 , but rather a background density that decreases with height [pressure]

⇒ a background of constant

Potential Temperature

General Thermal Energy Equation

$$\rho c_v \frac{DT}{Dt} = -\nabla \cdot \underline{q} - p \nabla \cdot \underline{u} + \underline{\tau} : \nabla \underline{u}$$

$$= -\nabla \cdot \underline{q} + \frac{p}{\rho} \frac{D\rho}{Dt} \quad \left[\begin{array}{l} \text{mass} \\ \text{conservation} \end{array} \right]$$

$$= -\nabla \cdot \underline{q} - p\rho \left[\frac{1}{\rho^2} \frac{D\rho}{Dt} \right] = -\nabla \cdot \underline{q} - p\rho \frac{D}{Dt} \left[\frac{1}{\rho} \right]$$

Ideal Gas

$$p = \rho RT$$

$$\rho c_v \frac{DT}{Dt} = -\nabla \cdot \underline{q} - p\rho \frac{D}{Dt} \left[\frac{RT}{p} \right]$$

$$= -\nabla \cdot \underline{q} - \frac{p\rho R}{p} \frac{DT}{Dt} + \frac{p\rho RT}{p^2} \frac{Dp}{Dt}$$

$$= -\nabla \cdot \underline{q} - \rho R \frac{DT}{Dt} + \frac{Dp}{Dt}$$

$$\rho c_p \frac{DT}{Dt} = -\nabla \cdot \underline{q} + \frac{Dp}{Dt}$$

Boussinesq assumes $\frac{Dp}{Dt}$ small

Divide by ρT :

$$\frac{c_p}{T} \frac{DT}{Dt} = - \frac{\nabla \cdot \mathbf{q}}{\rho T} + \frac{R}{P} \frac{DP}{Dt}$$

$$c_p \frac{D \ln T}{Dt} - R \frac{D \ln P}{Dt} = - \frac{\nabla \cdot \mathbf{q}}{\rho T}$$

Introduce Potential Temperature $\theta = T \left(\frac{P_s}{P} \right)^{\frac{R}{c_p}}$

not to be confused with the notation θ in the previous notes !!

P_s = surface pressure

θ = temperature a parcel would have if it moves adiabatically [no heat leaves the parcel] from its current height down to the surface.

$$\ln \theta = \ln T + \frac{R}{c_p} [\ln P_s - \ln P]$$

$$C_p \ln \theta = C_p \ln T - R \ln p_s - R \ln p$$

$$C_p \frac{D}{Dt} \ln \theta = C_p \frac{D}{Dt} \ln T - R \frac{D}{Dt} \ln p$$

$$= - \frac{\nabla \cdot \mathbf{q}}{\rho T}$$

2^{nd} Law of Thermodynamics

$$\delta Q = T dS, \quad \frac{\delta Q}{\delta t} = - \frac{\nabla \cdot \mathbf{q}}{\rho}$$

$$\frac{1}{T} \frac{\delta Q}{\delta t} = \frac{dS}{dt} = - \frac{\nabla \cdot \mathbf{q}}{\rho T}$$

\Rightarrow surfaces of constant θ are surfaces of constant entropy

* the natural background state is one of constant θ [not constant ρ]

Finally

$$\frac{D\theta}{Dt} = \frac{\theta}{T} \left(\frac{\kappa}{\rho c_p} \right) \nabla^2 T$$